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Pure aromatics from biomass

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Pure aromatics from biomass

Biorefinery I: Chemicals and Materials From Thermo-Chemical Biomass Conversion and Related Processes

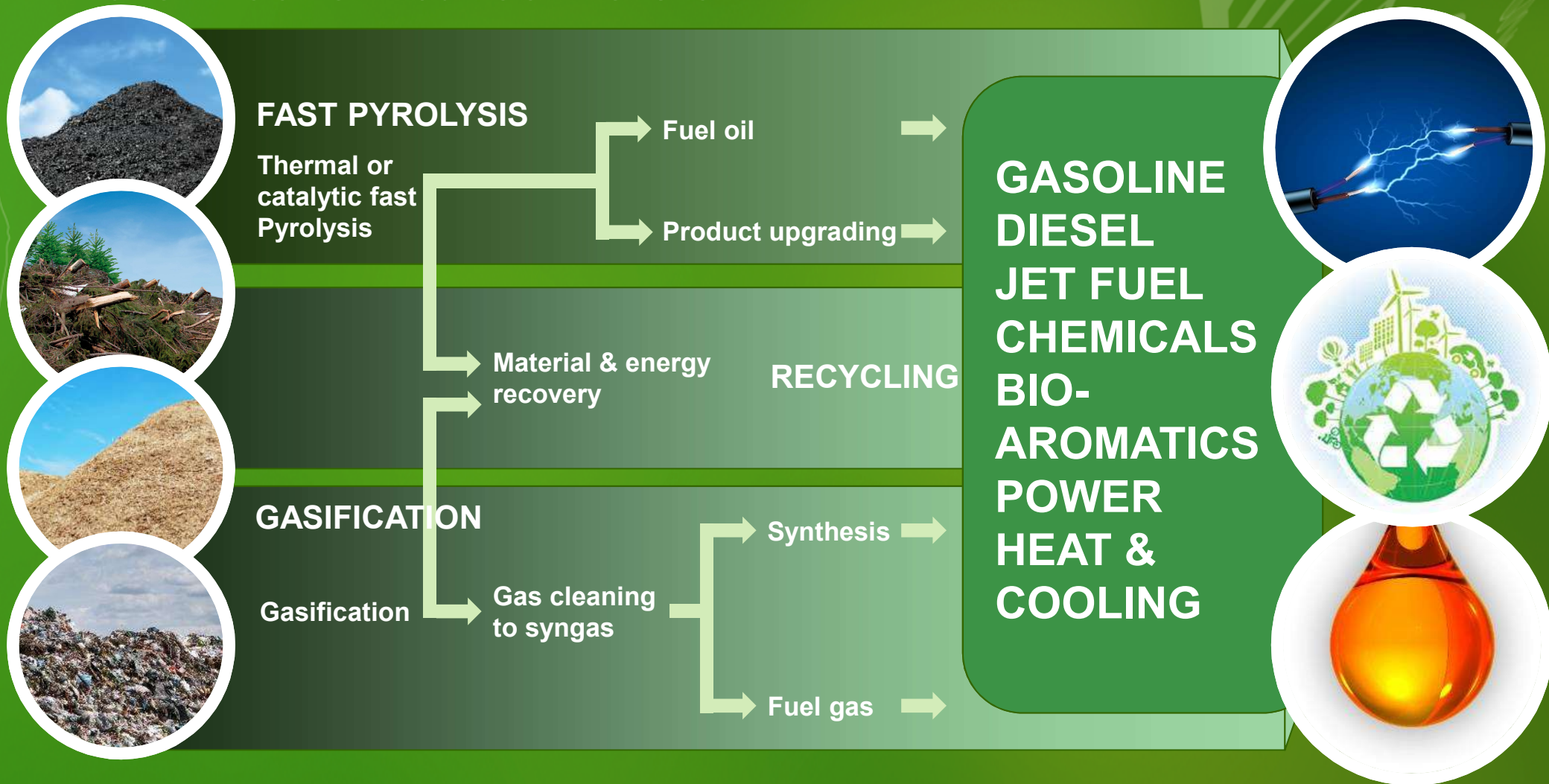
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Outline

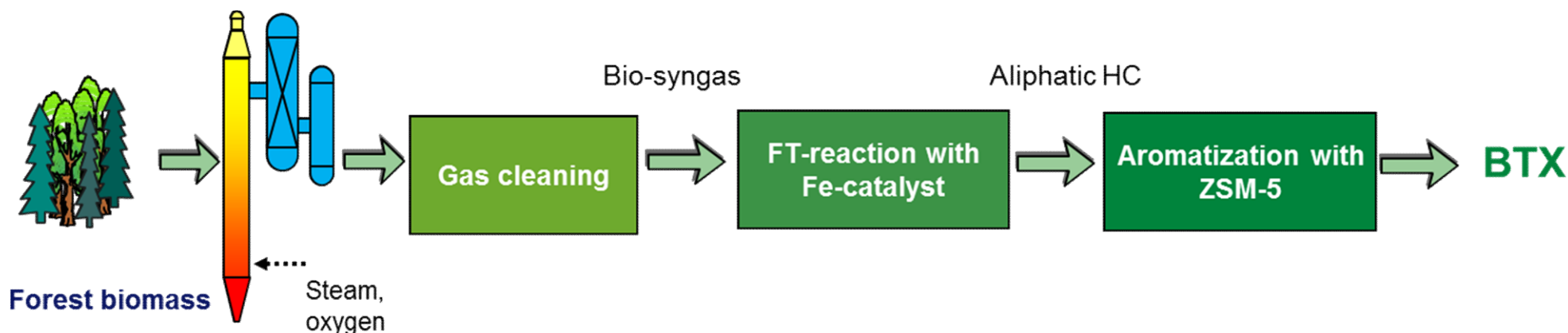
- Background /introduction
 - Why BTX via biomass gasification ?
 - Description of the process
- Laboratory scale experiments
 - Catalysts and reactor system
 - Product distribution, and separation of pure compounds
 - Example of a synthesis of an end-product
- Cost estimates for large scale production
- Next steps
- Conclusions

Thermochemical conversion: High-value products, low carbon energy and material recycling via thermochemical conversion



Biomass gasification route to BTX-chemicals

- BTL-process to diesel has been successfully demonstrated. However, there aren't any commercial plants
- As an alternative, we propose a cheaper process to valuable aromatic chemicals
- Competing technologies such as catalytic pyrolysis often suffer from bad selectivity – a mixture of phenols, methoxyphenols and substituted aromatics is of little value as a starting material for syntheses
- Principle of the process:

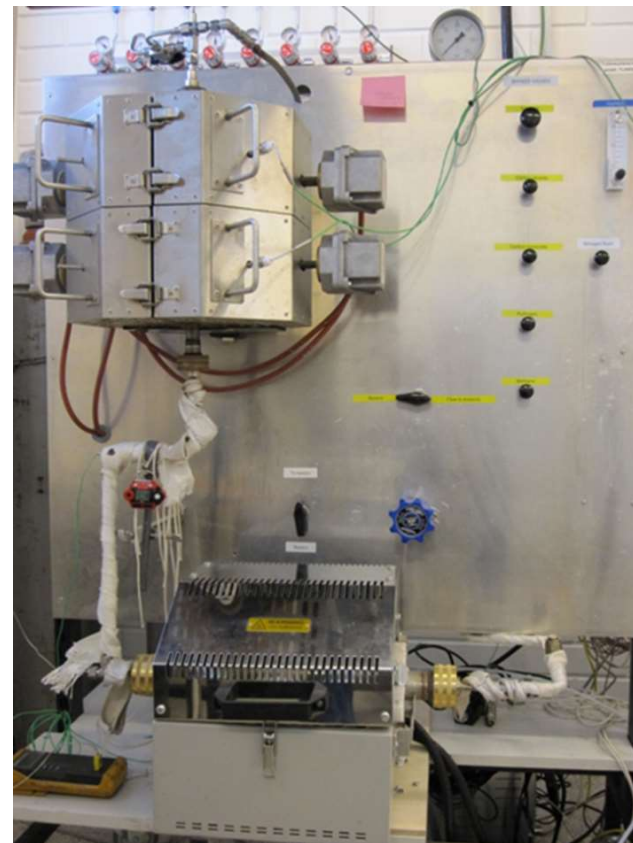


Laboratory scale experiments

A two-stage process:

- a) Fischer-Tropsch-reaction over precipitated iron catalyst 100Fe:4.6Si:2.0Cu:1.4K (atom ratio)¹. $H_2/CO = 1.4$ mol/mol. Temperature 200 – 300°C, pressure 0.1 – 0.5 MPa.
- b) Aromatization over ZSM-5 promoted by Zn (0.6 %) and La (0.8 %). Temperature 400 – 500°C, pressure 0.1 MPa.

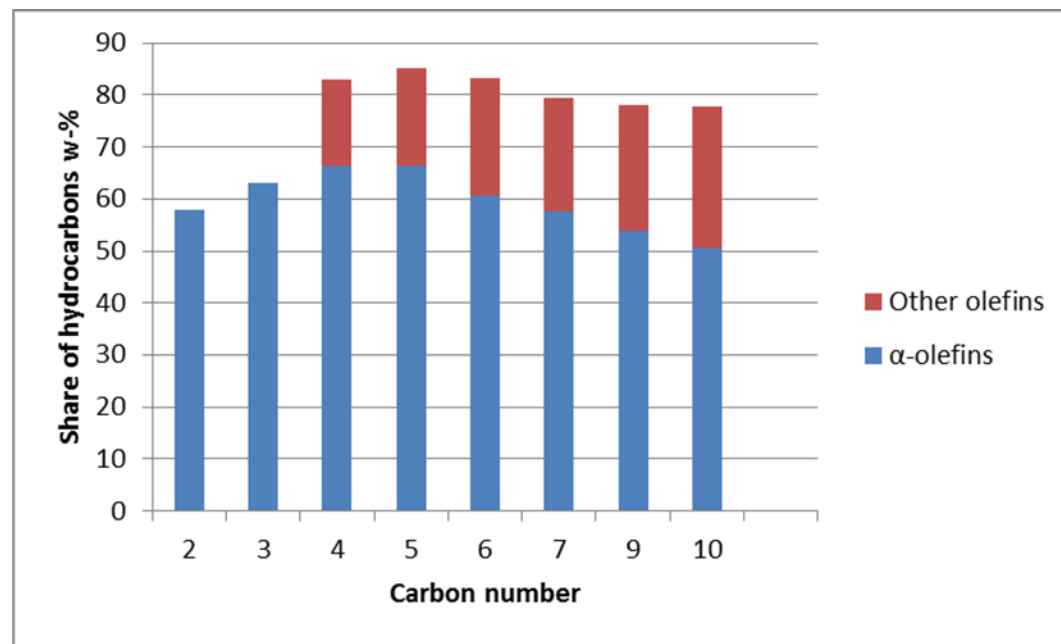
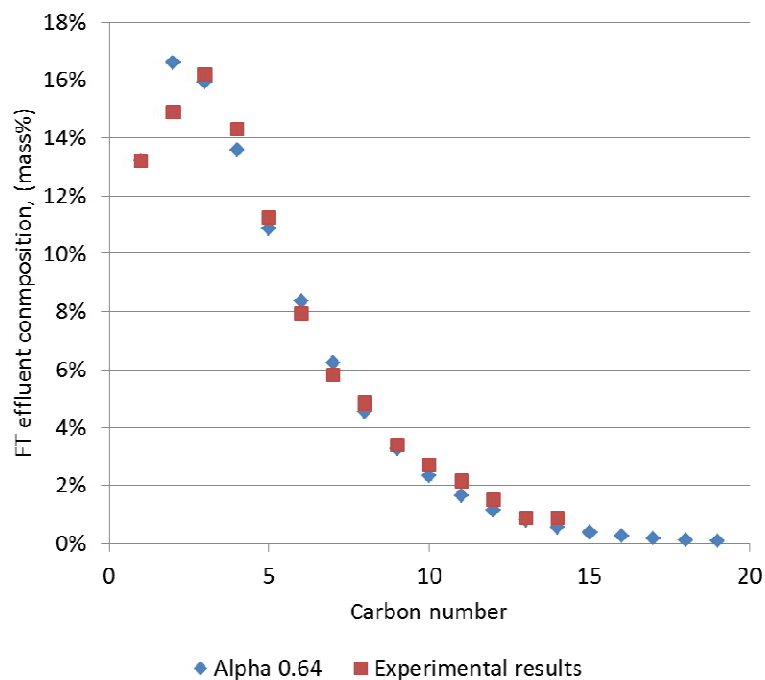
Simple tubular reactors connected directly in series, on-line GC-analysis



¹ Catal. Lett. (2013) 143, 1123-1131

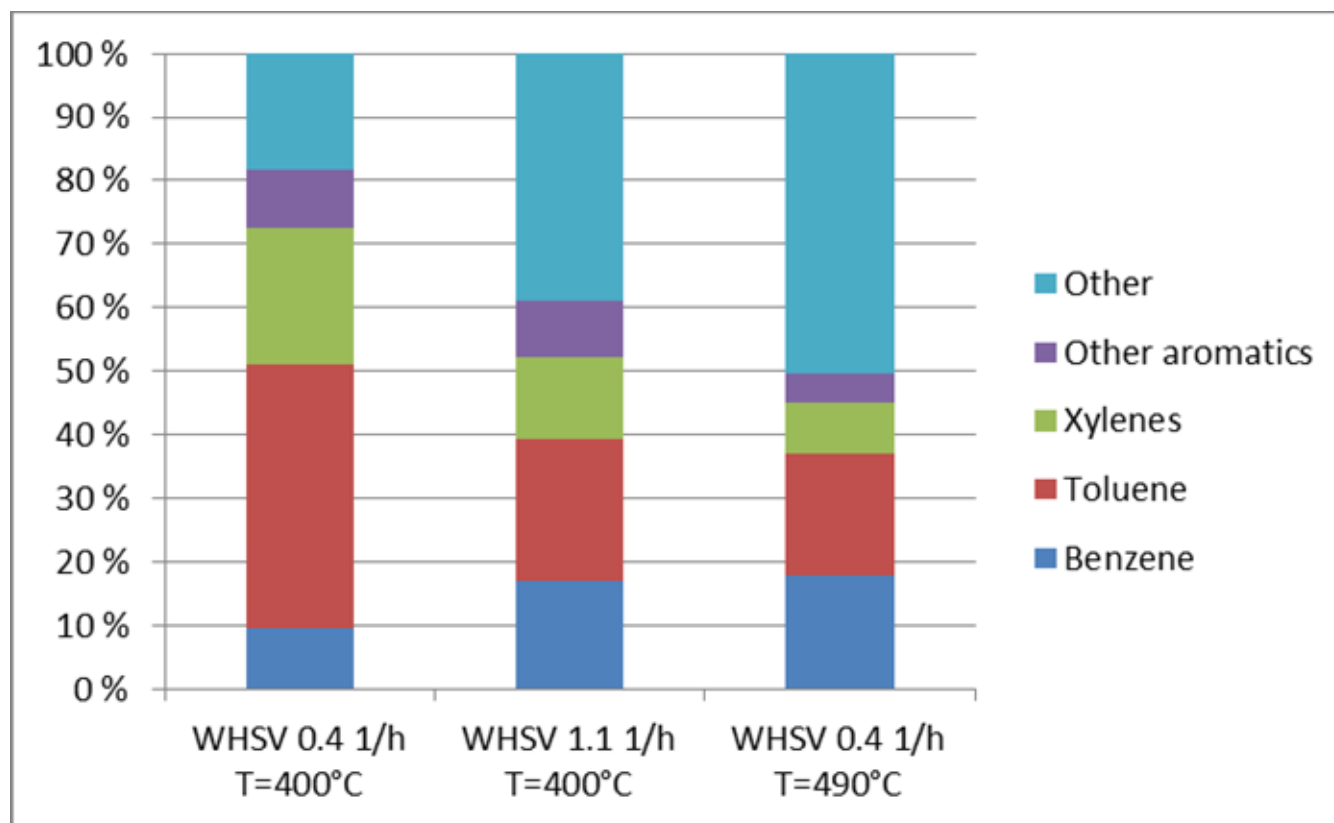
² Chi. J. Chem. Eng. (2011) 19,439-445

Step 1: FT reaction



FT-reaction step: $H_2/CO=1.4$ (mol/mol), 240°C, 0.1 MPa, WHSV=1.3 1/h, $\alpha=0.64$, CO conversion 64 %

Step 2: The effect of aromatization conditions



FT-reaction step: $\text{H}_2/\text{CO}=1.4$ (mol/mol), 240°C , 0.1 MPa, $\text{WHSV}=1.3$ h^{-1} , $\alpha=0.64$.

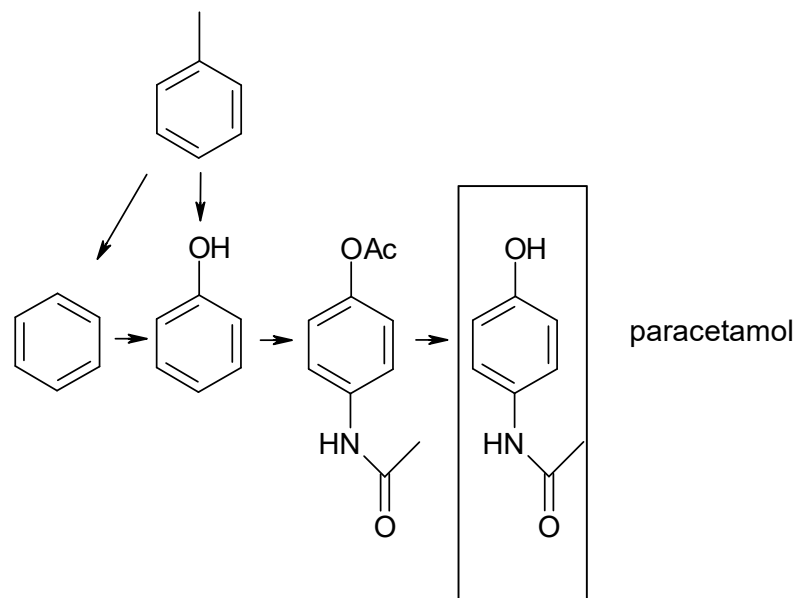
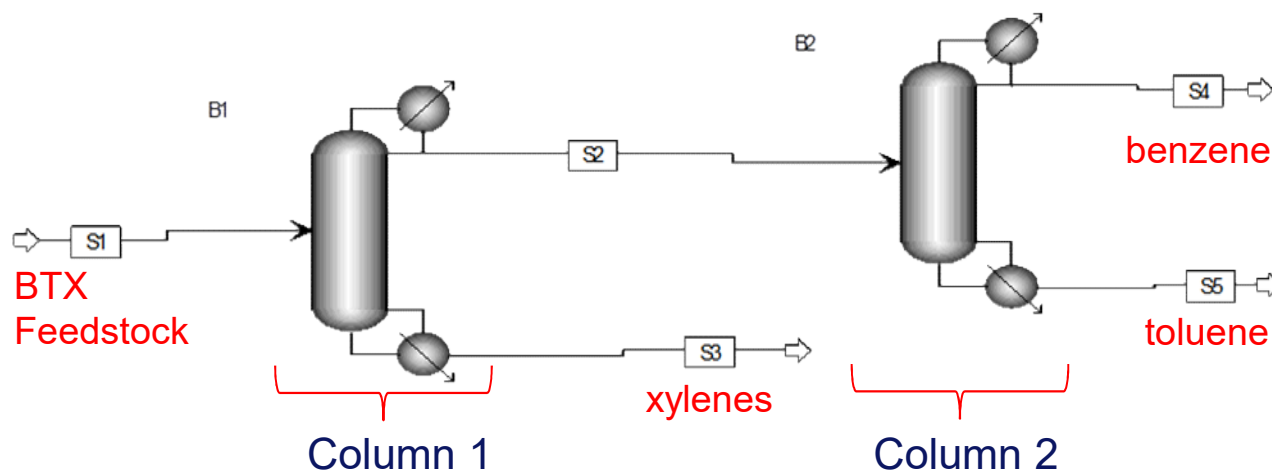
Composition of the reaction product (w-%)

Product	WHSV 0.4 h ⁻¹ T=400°C	WHSV 1.1 h ⁻¹ T=400°C	WHSV 0.4 h ⁻¹ T=490°C
CO ₂	2.6	4.2	6.9
CH ₄	11.4	8.3	11.1
C2	2.9	16.2	19.2
C3	0.7	5.4	8.1
C4	0.5	4.1	4.2
C5	0.1	0.5	0.5
C6	0.0	0.1	0.3
Benzene	9.4	17.1	18.0
Toluene	41.5	22.2	19.0
Xylenes	21.5	13.0	8.0
C3-Benzene	8.6	7.2	3.7
C4-Benzene	0.4	0.7	0.3
Naphthalene	0.3	0.8	0.8
Methylnaphthalene	0.0	0.2	0.0
Dimethylnaphthalene	0.0	0.0	0.0
Total aromatics	81.8	61.2	49.8

FT-reaction step: H₂/CO=1.4 mol/mol, 240°C, 0.1 MPa, WHSV=1.3 h⁻¹, α=0.64

Isolation of pure compounds for synthesis

- In large scale, according to ASPEN-modelling, a two distillation column set-up produces almost **pure benzene and toluene** fractions.
- In laboratory BTX-compounds were separated using Vigreux distillation followed by crystallisation
- As an example of synthesis, bio-paracetamol was synthesised from the separated benzene and toluene fractions



How much does it cost ?



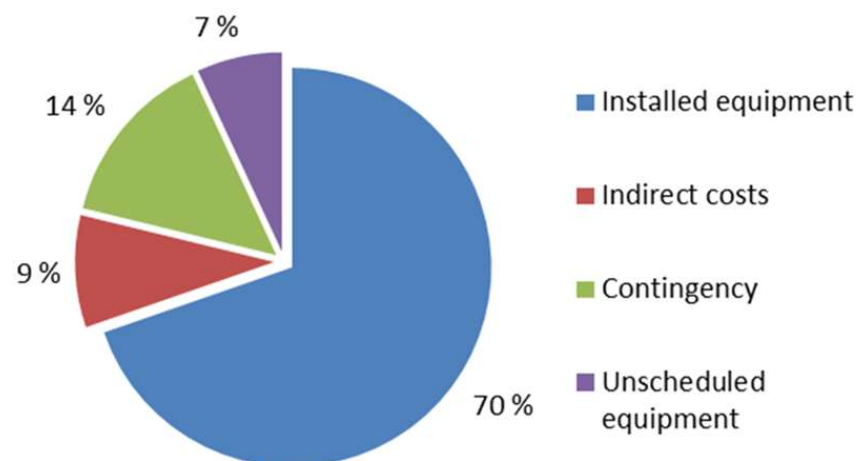
Base Case plant

- Biomass input 1000 dry MTPD (~200 MWth)
- Bio-BTX output 64 kton/a
(192 MTPD = 16 % mass yield)

Cost estimates

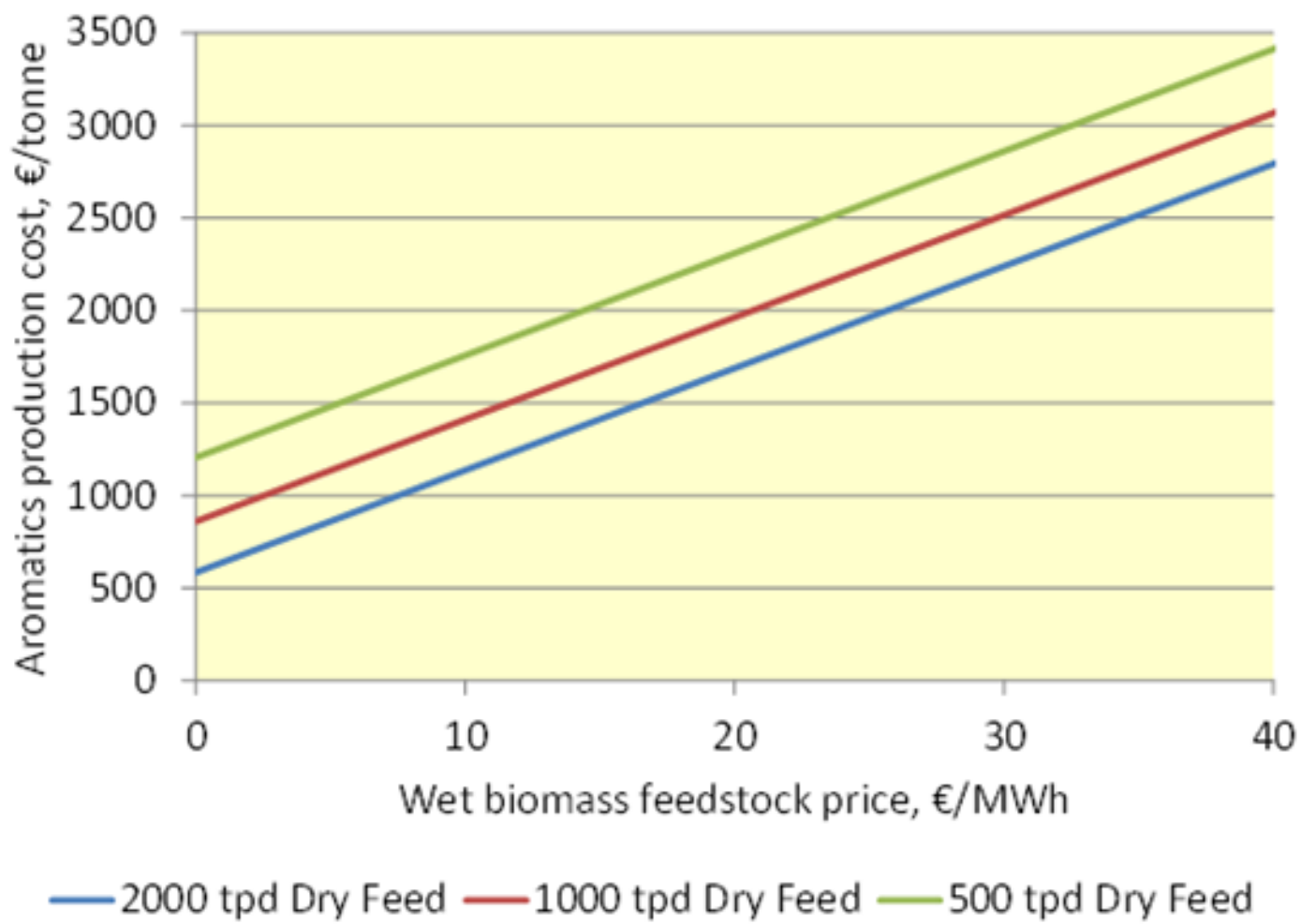
- Syngas plant = 231 M€
- OT FT-aromatics island = 37 M€
- TOC = 268 M€

Breakdown of investment costs



More on cost calculation methodology in a recent VTT publication which can be downloaded at <http://bit.ly/192VI3G>

Production cost of aromatics vs. biomass price and plant capacity



Conclusions

- We have shown that pure BTX components can be synthesized from biomass derived gas and isolated in high purity. The first estimate of the production cost of bioaromatics is about 1.4 €/kg.
- Bio-BTX can be used as a starting material for demanding end-products such as bio-paracetamol.
- Despite its selectivity the process is a multi-product process
- The next step is to scale-up the process at VTT's new Bioruukki-piloting facility to demonstrate the whole chain of bio-aromatics production "from stump to the final product".



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