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Effect of the variable porosity on the heat transfer process in solar air receiver

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EFFECT OF THE VARIABLE POROSITY ON THE HEAT TRANSFER PROCESS IN SOLAR AIR RECEIVER

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ABSTRACT

Solar air receiver is the core component of central receiver system (CRS) in solar thermal power plants due to the unique feature of some porous medium like silicon carbide foam ceramic and so on. In the air receiver, the porous material receives the concentrated sunlight from the heliostat field and heats up the pumped inlet air by convection and radiation. The incident radiation is distributed in the inner space of the porous medium rather than located on the boundary of the heated face in the front of the receiver. Aiming at this phenomenon which called volumetric effect, we propose a novel solar air receiver using the porous medium with variable porosity along the incident direction to optimize its heat transfer process and increase the thermal efficiency of the receiver. For this kind of porous medium, the effect of the variability of the porosity $\square$ on the temperature and radiative heat flux distributions and also the thermal efficiency of the air receiver will be analyzed systematically. Our analysis demonstrated that the structure with variable porosity will enhance the transfer of radiative energy into the porous medium, consequently decreases the thermal radiative loss at the inlet and increases the thermal efficiency of the air receiver.

INTRODUCTION

Porous media is widely utilized in many modern industrial applications involving heat transfer processes such as solar thermal utilization, nuclear waste repository, heat pipes, combustion, heat transfer enhancement etc. One area of utilization is the receiver (Aacutevila AL 2011) of a central receiver system (CRS) in solar thermal power plants due to the unique feature of silicon carbide (SiC) foam ceramic, such as large specific area, high conductivity and thermal shock resistance. In CRS, the porous material receives the concentrated sunlight from the heliostat field and heats up the pumped inlet air by convection and radiation.

Investigate on variants in local thermal non-equilibrium model was given by (Alazmi B, Vafai K 2000) considering the effect of non-Darcy, dispersion, non-equilibrium and variable porosity. The effect of different boundary conditions under LTNE conditions was given by (Yang K, Vafai K 2010). However for the high temperature over thousands, thermal radiation behavior can not be neglected. Its impact on conductive heat transfer in a packed bed has been analyzed by (Singh BP, Kaviany M 1991). Aim at the radiation transfer in the porous media in some typical industrial device, (Wang P, Vafai K, and Liu DY 2014) performed a numerical analysis focus on the LTNE model coupled with radiation transfer. The mechanism of the influence of the radiation transfer on the coupled heat transfer process with conduction and convection in the media was revealed; (Flamant G, Olalde G 1983) focus on the radiation heat transfer process in a double layers structure (glass bed and SiC porous layer) experimentally.

When considering the collimated incident radiation, the distribution of radiative energy changes in the incident direction should be taken into account simultaneously with convection processes. Hence, the purpose of this study is to understand the role of the collimated incident radiation on the convective heat transfer in air receiver under LTNE conditions. In this work, the temperature fields for the solid matrix and fluid phases will be analyzed while incorporating the local thermal non-equilibrium along with the differential approximation (P-1 model). The effect of intrinsic properties and optic parameters will be discussed respectively.

NOMENCLATURE

c_p	Specific heat of fluid at constant pressure [J kg^{-1} K^{-1}]
d_p	Pore diameter [m]
E_b	Blackbody emissive power
F	Inertial coefficient
G	Incident radiation
h_v	Volumetric heat transfer coefficient [W m^{-2} K]
J	Radiosity
K	Permeability [m^2]
L_a	Thickness of a absorber [m]
$\dot{m}$	Mass flow rate [kg/s/m^2]

P	Pressure [Pa]
Pr	Prandtl number
q_0	Initial heat flux [W/m^{-2}]
q	Heat flux
$\hat{s}$	Unit vector in the direction of fluid flow
T	Temperature [K]
u	Velocity[m/s]
V	Velocity vector [m s^{-1}]

Greek symbols:

α_{sf}	Specific surface area of the porous medium [m^{-1}]
ε	Emissivity
φ	Porosity
λ	Thermal conductivity [W m^{-1} K^{-1}]
μ	Dynamic viscosity [kg m^{-1} s^{-1}]
β	Extinction coefficient [m^{-1}]
τ	Optic thickness
ω	Single scattering albedo
Ψ	Dimensionless heat flux

subscripts

a	Average/absorber
b	Back
c	Collimated/cavity
d	Diffuse
e	Effective/environment
f	Fluid phase
r	Radiative
s	Solid phase
t	Total
v	Void
w	Wall

2 Model description

2.1 Physical model and assumptions

Figure 1 shows the schematic structure of a SiC ceramic foam air receiver or volumetric receiver is used to receive concentrated flux on its surface which is cooled directly by the pumped air. As can be seen the receiver's surface area (y direction) is much larger than its thickness (x direction). As such a one dimensional approximation in the direction of the thickness is invoked. We will also assume that the solid matrix is homogeneous and isotropic, and the variations of the thermal properties of solid and fluid phases are neglected. Furthermore the flow is considered to be steady and fully developed.
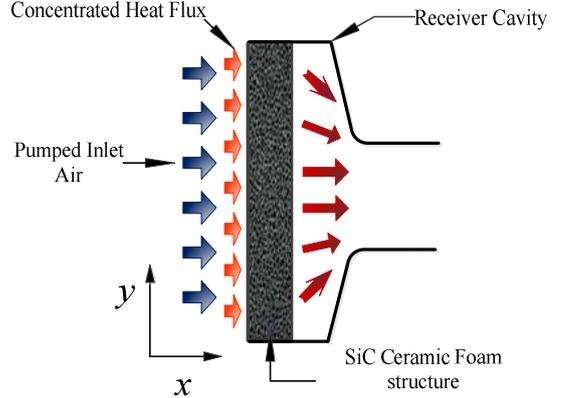

Figure 1: Schematic of the SiC ceramic foams air receiver

2.2 Mathematical model

2.2.1 Governing Equations

Continuum equation：
$$\nabla \langle V \rangle = 0 \tag{1}$$

Momentum equation：
$$\frac{\rho_f}{\varphi}\langle (V \cdot \nabla)V \rangle = \frac{\mu_f}{\varphi}\nabla^2 \langle V \rangle - \nabla \langle P \rangle^f - \frac{\mu_f}{K}\langle V \rangle - \frac{\rho_f F \varphi}{\sqrt{K}}\left[\langle V \rangle \cdot \langle V \rangle\right]J \tag{2}$$

where the permeability K, empirical function F which depends primarily on the microstructure of the porous medium can be represented as:

$$K = \frac{\varphi^3 d_p^2}{150(1-\varphi)^2} \tag{3}$$

$$F = \frac{1.75}{\left(150\varphi^{3/2}\right)^{1/2}} \tag{4}$$

and $\langle P \rangle^f$ is the gauge pressure and the local volume average of a quantity Φ can be defined as $\langle \Phi \rangle \equiv \frac{1}{V_f}\int_{V_f}\Phi dV$, J is a unit vector oriented along the velocity vector.

Energy equations:
fluid phases:
$$(\rho c_p)_f \langle V \rangle \cdot \nabla \langle T_f \rangle = \nabla(\lambda_{fe} \cdot \nabla \langle T_f \rangle) + h_{sf}a_{sf}(\langle T_s \rangle - \langle T_f \rangle) \tag{5}$$

solid phases:
$$0 = \nabla \cdot (\lambda_{se} \cdot \nabla \langle T_s \rangle - q_r) - h_{sf}a_{sf}(\langle T_s \rangle - \langle T_f \rangle) \tag{6}$$

where:

$$\lambda_{\text{fe}} = \varphi \lambda_{\text{f}} \tag{7}$$

$$\lambda_{\text{se}} = \varphi \lambda_{\text{s}} \tag{8}$$

The specific surface area of porous bed with appears in both energy equation 5 and 6 is developed based on geometrical considerations:

$$\frac{6(1-\varphi)}{d_{\text{p}}} \tag{9}$$

The fluid-to-solid phase heat transfer coefficient in this study was based on the empirical correlation established by (Wang P, 2015) is presented as follows:

$$h_{\text{sf}} = \left(\frac{d_{\text{p}}\varphi}{0.2555 Pr^{1/3} Re^{2/3} \lambda_{\text{f}}} + \frac{d_{\text{p}}}{10\lambda_{\text{s}}} \right)^{-1} \tag{10}$$

The radiation parameters that is the extinction β, absorption κ and scattering coefficients σ_{s} are strongly dependent on the experimental test. (Hsu Pf, Howell JR 1992) presented a method of simultaneously inverting conductivity and extinction coefficient from the experimental data. The trend of the change of extinction coefficient had good agreement the geometric optics limit prediction (Tien CL 1988) when pore size greater than 0.6mm:

$$\beta = \frac{\Psi}{d_{\text{p}}}(1-\varphi) \tag{11}$$

where the value of Ψ is given as 3, other test results shows that Ψ should be change to 4.4 based on foam ceramic porous media. (Mohanraj R *et. al.* 1996) also presented the experimental test focus on the RPC material, the result shows that radiation properties is not sensitive to the temperature at the range of 1200K-1400K, detailed parameters is given as follow:

$$\kappa = (2-\varepsilon)\frac{3}{2d_{\text{p}}}(1-\varphi) \tag{12}$$

$$\sigma_{\text{s}} = \varepsilon \frac{3}{2d_{\text{p}}}(1-\varphi) \tag{13}$$

2.2.2 Radiation transfer

Under the assumption of collimated irradiation, a modified differential approximation (P-1 Model) is applied to address this problem here. We have the express for the diffuse radiative flux q_{d} and the incident radiation G_{d} as follow:

$$\nabla q_{\text{d}} = \kappa \left(4\sigma \langle T_{\text{s}} \rangle^4 - G_{\text{d}} \right) + \sigma_{\text{s}} G_{\text{c}} \tag{14}$$

$$q_{\text{d}} = -\frac{1}{3\beta} \nabla G_{\text{d}} \tag{15}$$

Then the differential equation for G_{d} is obtained as:

$$0 = \frac{1}{3\beta} \nabla G_{\text{d}}^2 + \kappa \left(4\sigma \langle T_{\text{s}} \rangle^4 - G_{\text{d}} \right) + \sigma_{\text{s}} G_{\text{c}} \tag{16}$$

Meanwhile q_{c}, the remnant collimated beam after partial extinction, by absorption and scattering, along its path in the direction which perpendicular to the horizontal boundary is given by the exact solution:

$$q_{\text{c}} = G_{\text{c}} = q_0 e^{-\beta x} \tag{17}$$

2.2.3 Variable porosity

The variation of the porosity in the flow direction are defined by a linear function:

$$\varphi = A_{\text{p}} + (B_{\text{p}}/L_{\text{a}}) \cdot x \tag{18}$$

where the coefficient A_{p} and B_{p} control the variation of the porosity. When the B_{p} is negative, it means that the porosity decreases along the flow direction, however it increase when B_{p} is positive.

2.2.4 Boundary conditions

The incident radiation flux q_{in} which is concentrated by a heliostat field can be presented by:

$$q_{\text{in}} = 1MW/m^2 \tag{19}$$

Radiation heat loss between the receiver's surface and environment can be represented by:

$$q_{\text{loss}} = \sigma\varepsilon \left(\langle T_{\text{s,in}} \rangle^4 - \langle T_{\text{e}} \rangle^4 \right) \tag{20}$$

The temperature of the inlet fluid, $T_{\text{f,in}}$ is the same as the environment temperature T_{e} which is taken as

$$T_{\text{f,in}} = T_{\text{e}} = 300K \tag{21}$$

For the outlet boundary, an adiabatic boundary condition is used:

$$\frac{\partial \langle T_{\text{s}} \rangle}{\partial x} \bigg|_{x=L} = 0 \tag{22}$$

$$\frac{\partial \langle T_{\text{f}} \rangle}{\partial x} \bigg|_{x=L} = 0 \tag{23}$$

the diffuse radiative flux can be neglected hence the radiative boundary conditions for the

inlet and outlet are as follows:

$$\left.\frac{\partial \langle G_{\mathrm{d}} \rangle}{\partial x}\right|_{x=0} = \left.\frac{\partial \langle G_{\mathrm{d}} \rangle}{\partial x}\right|_{x=L} = 0 \qquad (24)$$

3 Numerical procedure

Using a Finite Volume Method, Governing equations are discretized using a SIMPLE algorithm. The discretization scheme is based on a uniform grid set up and a cell centered scheme. Furthermore, 1st order upwind differencing method is employed to discretize the convective terms. The convergence is considered to have been reached when the relative variation of temperature between consecutive iterations is smaller than 10^{-8} for all the grid points in the computational domain.

4 Results and discussion

4.1 Increasing porosity

Fig. 2 depicts the distribution of fluid and solid temperature T_{f} and T_{s} and heat flux q for different value of porosity φ with constant pore diameter d_{p}=2mm, inlet air velocity U_{in}=0.5m/s and incident radiation q_0=1MW.

As expected in the Fig. 2a and 2b, the temperature T_{s} along the x direction for the solid phase is decrease in the incident direction, however, for the fluid phase temperature T_{f}, it increases along the x direction. It can be seen that the solid temperature T_{s} at the irradiated surface greatly decreases when using the variable porosity material along the x direction. T_{s} decreases nearly 50K when the control parameters A_{p}=0.9 and B_{p}=-0.3. The outlet air temperature at the back wall of the absorber increases when using the variable porosity material, this is because that the lower surface temperature decreases the radiative loss, consequently the efficiency increased accordingly.

Fig. 3a, and 3b present that both of the variation value of the extinct collimated radiative flux q_{c}, diffuse radiative flux q_{d} and conductive heat flux q_{s} along the x direction. It can be seen that the incident radiative energy here we assume as the gradient of the collimated

irradiation attenuation decreases sharply along the incident direction of the porous media. This part can be taken as the volumetric energy source distributed in the porous media. Hence, with its decrease the heat flux absorbed by the porous media decreases. However the diffuse radiative q_{d} increases first and then decrease slightly, this is because the diffuse radiative flux q_{d} dependent on not only the solid temperature T_{s} but also the distribution of the incident irradiation q_{c}. For the conductive heat flux q_{s} in the solid phase *(see Fig. 3a, 3b)*, the effect of the porosity on its distribution has a reverse rule compared to that on the diffuse radiative flux. This shows the limiting interactions between thermal radiation and conduction. When comparing the Fig 3a, 3b we can also found that the conductive heat flux q_{s} decreases slightly at the irradiated surface.
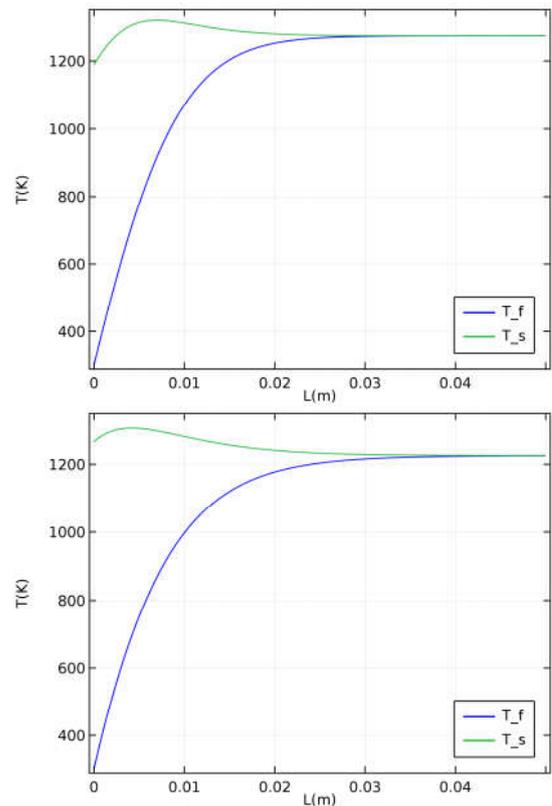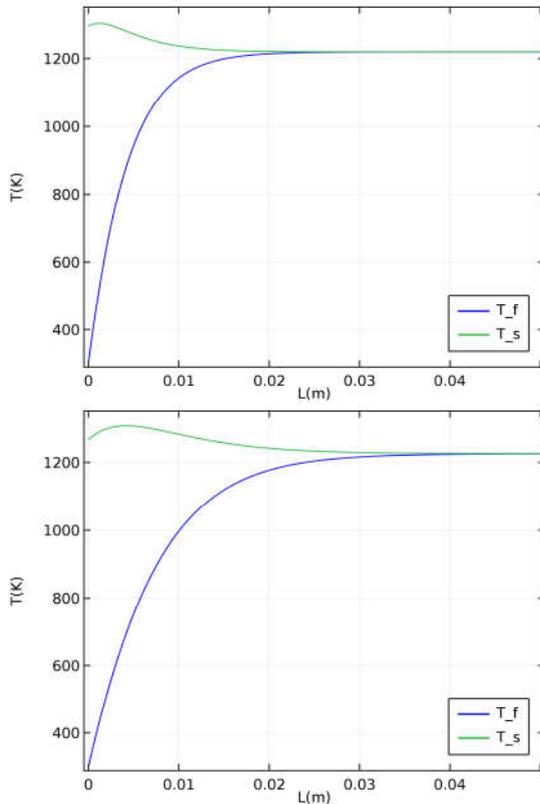

(a) Variable porosity (b) Constant porosity
Fig. 2: Effect of the porosity on the temperature and heat flux in the x direction (A_{p}=0.9, B_{p}=-0.3)
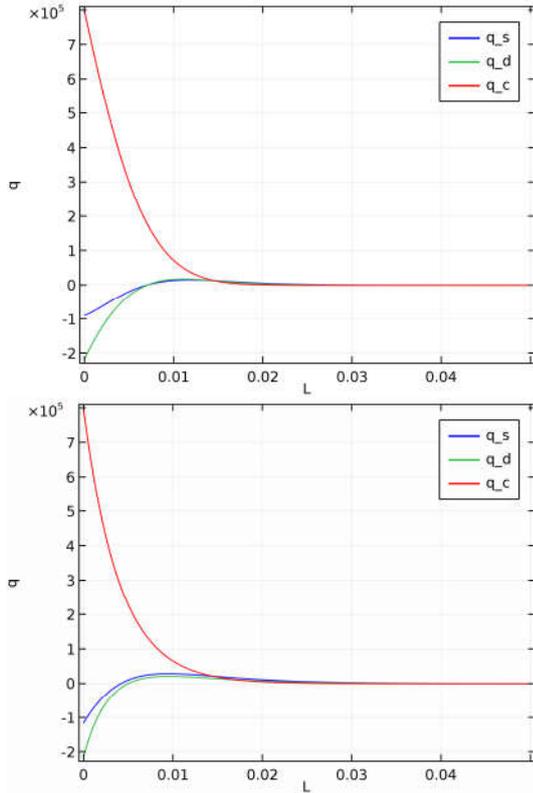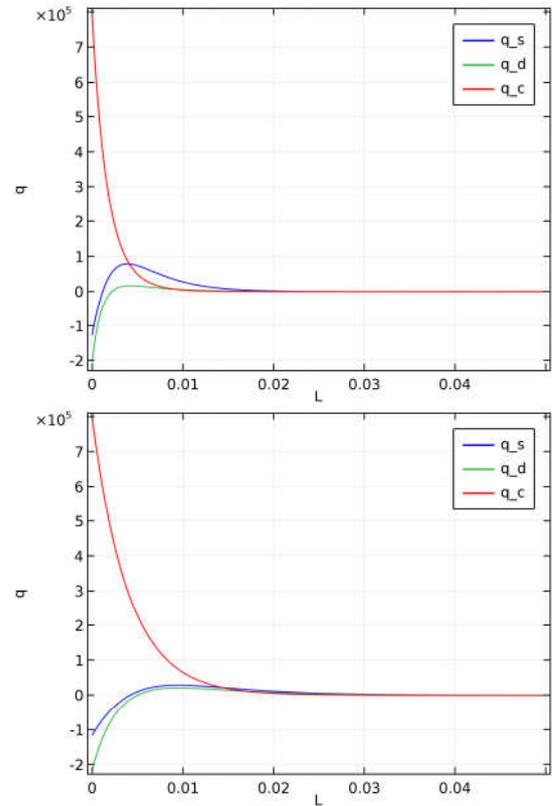
(a) Variable porosity (b) Constant porosity

Fig. 3: Effect of the porosity on the heat flux in the x direction (A_p=0.9, B_p=-0.3)

4.2 Decreasing porosity

(a) Variable porosity (b) Constant porosity

Fig. 5: Effect of the porosity on the heat flux in the X direction (A_p=0.9, B_p=-0.3)

Fig. 4 and 5 depicts the distribution of fluid and solid temperature T_f and T_s and heat flux q for different arrangement of porosity φ with constant pore diameter d_p=2mm, inlet air velocity U_{in}=0.5m/s and incident radiation q_0=1MW.

For this case, in the Fig. 4a and 4b, It can be seen that the solid temperature T_s at the irradiated surface greatly increases when using the variable porosity material along the x direction. T_s increases nearly 20K when the control parameters A_p=0.6 and B_p=0.3. The outlet air temperature at the back wall of the absorber decreases when using the variable porosity material, this is because that the lower surface temperature increases the radiative loss, consequently the efficiency decreased accordingly. When comparing the Fig 5a and 5b we can also found that the conductive heat flux q_s decreases more slightly at the irradiated

(a) Variable porosity (b)Constant porosity

surface for the variable porosity, which is due to the high temperature gradient of the solid phase with variable porosity effect.

CONCLUSIONS

Convective and radiative transport in a air receiver using porous media in the presence of collimated irradiation and local thermal non-equilibrium is analyzed in this work. A modified P-1 approximation with collimated irradiation was introduced to incorporate the radiative transfer. We analyzed the distribution of the temperature of the fluid and solid phase, also the heat flux in the incident direction was presented. Based on our analysis, it can be seen that the incident radiative energy i.e. the collimated irradiation attenuation sharply along the incident direction of the porous media. The temperature T_s along the x direction is decrease for the solid phase but increases for the fluid phase temperature T_f along the x direction. The diffuse radiative q_d increases first and then decrease, this is because the diffuse radiative flux not only dependent on the solid temperature but also the distribution of the incident irradiation i.e. the extinction part of collimated irradiation q_c. Lower solid temperature can be achieved by using a variable porosity. The porosity and pore diameter has a non-monotonic effect on the thermal efficiency of the receiver, optimization can be achieved by further parameters analysis.

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