Engineering Conferences International ECI Digital Archives

Fluidization XV

Proceedings

5-23-2016

Heat transfer challenge and design evaluation for a multi-stage temperature swing adsorption (TSA) process

Gerhard Hofer University of Natural Resources and Life Sciences, Austria, gerhard.hofer@boku.ac.at

Tobias Pröll University of Natural Resources and Life Sciences, Austria

Johannes Fuchs TU Wien, Institute of Chemical Engineering, Austria

Gerhard Schöny TU Wien, Institute of Chemical Engineering, Austria

Follow this and additional works at: http://dc.engconfintl.org/fluidization_xv Part of the <u>Chemical Engineering Commons</u>

Recommended Citation

Gerhard Hofer, Tobias Pröll, Johannes Fuchs, and Gerhard Schöny, "Heat transfer challenge and design evaluation for a multi-stage temperature swing adsorption (TSA) process" in "Fluidization XV", Jamal Chaouki, Ecole Polytechnique de Montreal, Canada Franco Berruti, Wewstern University, Canada Xiaotao Bi, UBC, Canada Ray Cocco, PSRI Inc. USA Eds, ECI Symposium Series, (2016). http://dc.engconfintl.org/fluidization_xv/42

This Abstract and Presentation is brought to you for free and open access by the Proceedings at ECI Digital Archives. It has been accepted for inclusion in Fluidization XV by an authorized administrator of ECI Digital Archives. For more information, please contact franco@bepress.com.



Heat transfer challenge and design evaluation for a multi-stage temperature swing adsorption (TSA) process

Gerhard Hofer*, Johannes Fuchs, Gerhard Schöny, Tobias Pröll

*gerhard.hofer@boku.ac.at

University of Natural Resources and Life Sciences (BOKU), Vienna

Department of Material Sciences and Process Engineering

Gerhard Hofer, University of Natural Resources and Life Sciences, Vienna

Content

- Introduction
- Problem definition
- Practical work
- Conclusion
- Outlook



Introduction Continuous CO₂ adsorption, TSA

Adsorption kinetics fast

 \rightarrow TSA limitation: Heat exchange (HEX)

- Contactors may be designed as fixed / moving bed
 →poor HEX rates!
- Solution: **Multi-stage bubbling fluidized bed** (BFB) columns with counter-current flow of gas & solids
- Considered particles: Geldart Type B





Introduction Continuous CO₂ adsorption, TSA

- Heat exchanger design: tube bundles
- Design parameters
 - Tube diameter (d_t)
 - Tube spacing (p_h, p_v)
 - Tube arrangement
 - Tube alignment
 - Tube surface



Fig. 2. Characteristical tube bundle design parameters



Problem definition | Pt.1

- Restricted BFB pressure drop Δp_{fb} | sf.gas velocity U →Limitation of installable HEX surface $(A_{HEX} \sim \Delta p_{fb} \sim 1/h)$
- Trade-off 1: $U \mid h$
- Trade-off 2: Heat exchanger design | h



Fig. 3. Calculated HEX rates for single tube (Molerus et al., 1995) and selected tube bundles (Lechner et al., 2013)

22

Problem definition Pt.2

- Resistance to particle flow
 - \rightarrow Tube alignment
 - \rightarrow Residence time dist. (RTD)
- Scale-up
 - \rightarrow Forces to tubes \rightarrow Durability
- Maintainability



Fig. 4. Horizontal tubes and particle flow possibilities (red = transversal, blue = longitudinal)



Practical work

- TSA needs most accurate heat exchanger design for efficient operation
- Evolved calculation models for single tube heat transfer rate available → significant quantity-differences (e.g. Martin, Molerus et al., ...)







6/3/2016

HTMT | Heat transfer measurement test device









Fig. 6. HTMT construction assembly

Conclusion

- Adsorption kinetics fast \rightarrow HEX limits TSA efficiency
- TSA heat exchanger design highly dependent on:
 - Restricted fluidized bed pressure drop
 - Intended superficial gas velocity
 - Scalability
 - Durability
 - Maintainability
- Heat transfer measurement test device successfully put into operation



Outlook

- HEX measurements with various
 - Bulk materials
 - Heat exchanger designs
- Investigate effect of tube bundles to residence time distribution (RTD) of particles
- Determine optimal tube bundle design for TSA



Questions & suggestions are appreciated!

Acknoledgements

The authors appreciate the financial support by the Austrian Climate and Energy Fund and gratefully acknowledge funding and publication permission from Shell Global Solutions International BV, The Hague.

References

Martin, H., (2013). Wärmeübergang in Wirbelschichten (chap. M5), VDI Wärmeatlas. Springer-Verlag, Berlin Heidelberg, 11th Ed., 2013. Molerus, O., Burschka, A., Dietz, S., (1995). Particle migration at solid surfaces and heat transfer in bubbling fluidized beds 2. Chemical Engineering Science 50 (5), 879-885. Lechner, S., Merzsch, M., Krautz, H.J., (2013). Heat-transfer from horizontal tube bundles into fluidized beds with Geldart A lignite particles. Powder Technology 253, 14-21.

