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A Novel Plant Cell Culture Platform for Semicontinuous Production of Recombinant Proteins: Butyrylcholinesterase as a Case Study

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Abstract

In this poster we describe a novel biomanufacturing production platform that utilizes transgenic rice cell suspension cultures for efficient semicontinuous cell culture production of recombinant proteins. This platform offers a number of advantages over traditional methods for production of recombinant therapeutic proteins that use *E. coli*, yeast or mammalian cell cultures, while still retaining the ability to meet cGMP regulatory requirements under well-controlled, reproducible production conditions. Results are presented for semicontinuous production of butyrylcholinesterase, a bioscavenger for organophosphorus nerve agents such as sarin, using metabolically regulated transgenic rice cell cultures in a 5 L bioreactor.

Background

Traditional methods for production of biologics use genetically modified *E. coli*, yeast, insect or mammalian cell cultures in bioreactor systems. For applications where a human therapeutic protein (monoclonal antibodies, vaccines, bioscavengers, replacement biologics) produced under strict cGMP conditions is required, plant cell cultures offer a number of advantages over currently used bioreactor-based systems:

- Low risk of contamination by mammalian viruses, bloodborne pathogens, prions or bacterial endotoxins or mycoplasma
- Ability to perform complex glycosylation
- Ease of culturing compared with other higher eukaryotic hosts
- Ability to grow in simple, low cost, chemically defined and animal component-free medium
- Established regulatory pathway for plant-based recombinant biologics for use as a human therapeutic

In the presented work, we focus on butyrylcholinesterase (BuChE) as a case study. BuChE is a tetrameric human enzyme that can act as a bioscavenger against organophosphorus nerve agents (Figure 1). Because of the high cost and limited availability of BuChE from human blood plasma, there is a need for a low cost, scalable recombinant platform for BuChE production.

Figure 1: The tetrametic form of BuChE is 340 kDa¹.



Conclusions

Confirmed multiple stable transgenic cell lines capable of

Successfully produced mg quantities of functional BuChE semi-

Induction #2 shows active BuChE present in the media at levels

comparable to active cell-associated BuChE in Induction #1.

Preliminary data indicate the production of tetrameric BuChE.

producing BuChE in a suspension culture.

continuously in a lab scale bioreactor.

Expression of the BuChE gene is controlled by the rice alpha amylase 3D promoter², which is activated by switching the rice from a sucrose-rich growth medium to a sucrose-free induction medium. This allows for a cyclical or semi-continuous culture operation that alternates between phases of cell growth (sugarrich) and expression (sugar-free). Gravity sedimentation within the bioreactor can be used to separate the plant cell aggregates from the liquid phase, and the product collected can be purified either using a batch downstream strategy or fed to a continuous downstream process.



Results: Semicontinuous Bioreactor Operation



Figure 6: Kinetic data from semicontinuous production of BuChE in transgenic rice cell cultures under controlled conditions of temperature (27°C), agitation (75 rpm), and dissolved oxygen (40% of saturation with air). in a 5 L bioreactor.

Figure 6a: Cell growth and oxygen uptake rate (OUR) kinetics.

Figure 6b: BuChE production and sugar consumption kinetics. Active BuChE concentration is determined by a modified Ellman activity assay³.



Optimization of bioreactor operating parameters, such as inoculation

density, aggregate size distribution, dissolved oxygen, temperature, pH,

and timing of induction in order to maximize culture health and

Evaluation of long-term (> 1 month) semicontinuous BuChE production.

Purification and biochemical characterization of rice cell culture-

volumetric productivity of functional BuChE.

produced BuChE and scale up of process.

	Growth Phase #1	Growth Phase #2
Maximum Specific Growth Rate (µ _{max})	0.17 ± 0.01 day ⁻¹	0.16 ± 0.02 day ⁻¹
Doubling Time (τ _D)	4.0 ± 0.2 days	4.4 ± 0.7 days

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	Expression Phase #1	Expression Phase #2
Active BuChE Yield	11.5 ± 0.1 µg/g FW	178.4 ± 23.6 µg/g FW
	0.306 ± 0.003 mg/L culture	8.4 ± 1.1 mg/L culture
Max Volumetric Productivity	16.1 ± 0.1 µg/(L⋅day)	954.8 ± 0.1 µg/(L·day)

Figure 7: Western blotting of rice cell culture-produced BuChE.

Figure 7a: Western blot under reducing conditions of cell-associated samples from before and after medium exchanges. Each lane contains 20 μ L of crude cell extract, obtained by grinding cells 1:1 in cold extraction buffer using a tissue homogenizer. Maximum BuChE expression occurs on day 5 after induction.

Figure 7b: Western blot under native conditions of 52 mU (~200ng) active BuChE from an intracellular sample from the first bioreactor expression phase (Induction #1). Tetrameric BuChE (~340 kDa) is observed.

2 Equine BuChE Contro

Figure 7b

Induction #1

Contents

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Future Work