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**Effects of Temperature and Residence Time on the  
Thermal Cracking of Bio-oil for Syngas Production**

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***Dynamotive***  
The Evolution of Energy



Western



# Introduction

- **Syngas:**
  - Mix of H<sub>2</sub> and CO
  - Can be used to synthesize chemicals and clean fuels
  - Now produced from fossil fuels such as natural gas
  
- **Producing syngas from biomass:**
  - Renewable resource
  - No net greenhouse gas emissions

# Introduction

- **Direct conversion of biomass to syngas:**
  - Simple
  - Transportation of biomass is expensive
- **Two stage process:**
  - 1) Local plants convert biomass to bio-oil
  - 2) Central plant converts bio-oil to syngas
  - Transportation is much easier
  - Valuable chemicals extracted from bio-oil

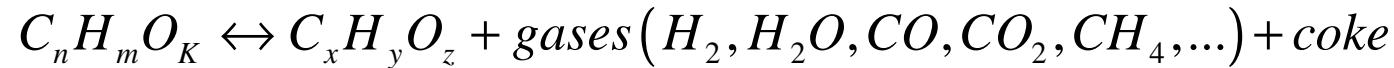
# Research Objectives

- Convert to syngas a bio-oil produced by Dynamotive from sawdust
- Thermal cracking of bio-oil in a hot fluidized bed of attrition-resistant silica sand

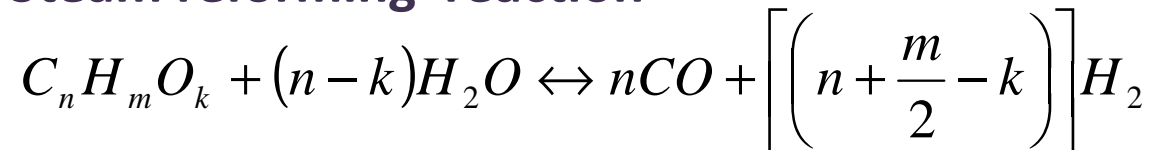


# Gasification Reactions

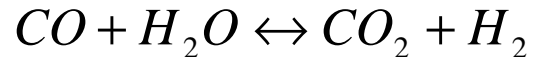
## ❑ Thermal cracking



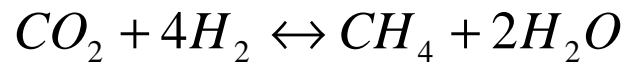
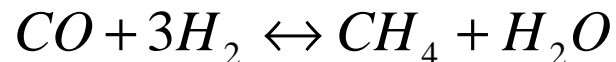
## ❑ Steam reforming reaction



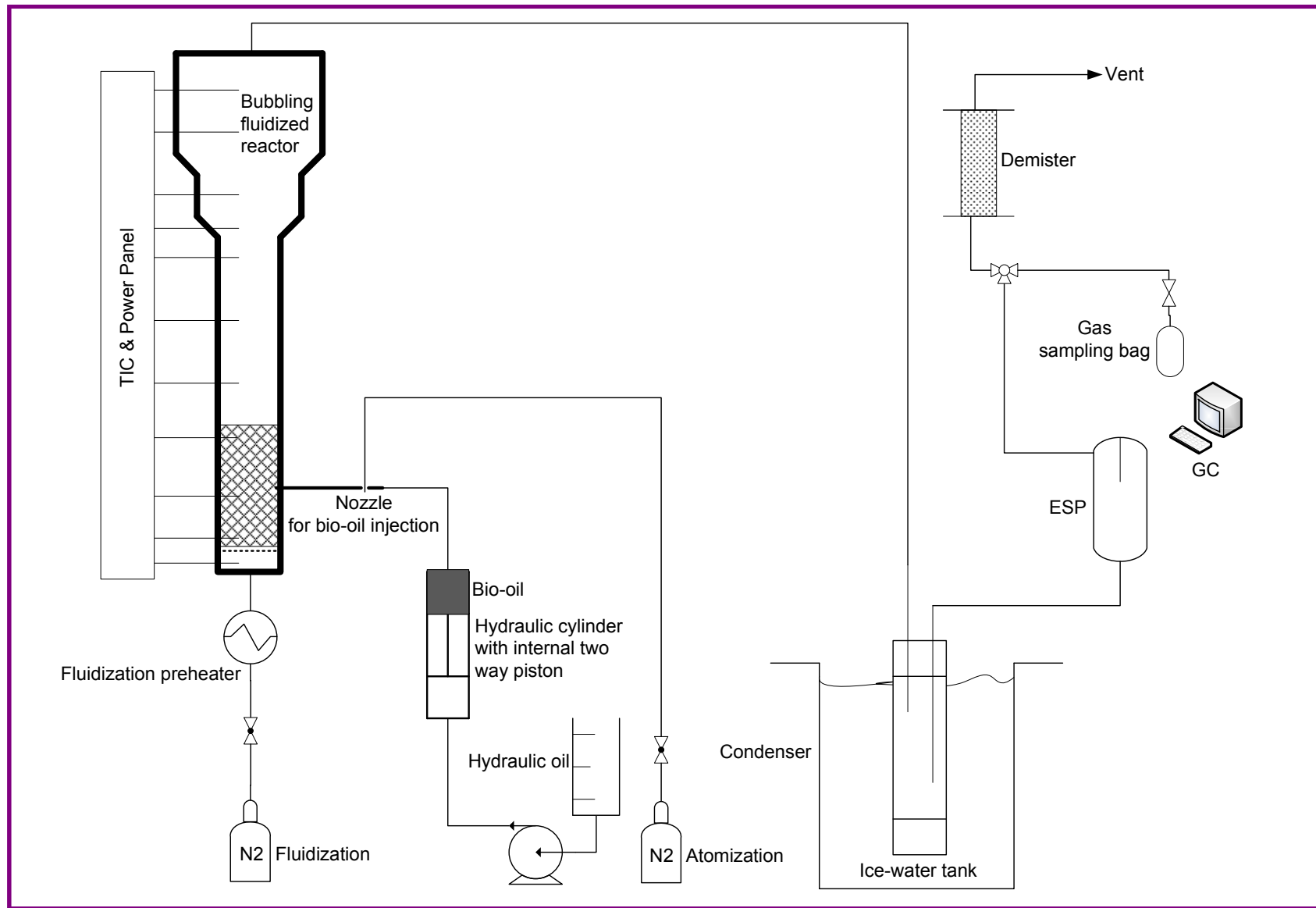
## ❑ Water gas shift reaction



## ❑ Methane formation



# Pilot Plant for Bio-oil Gasification

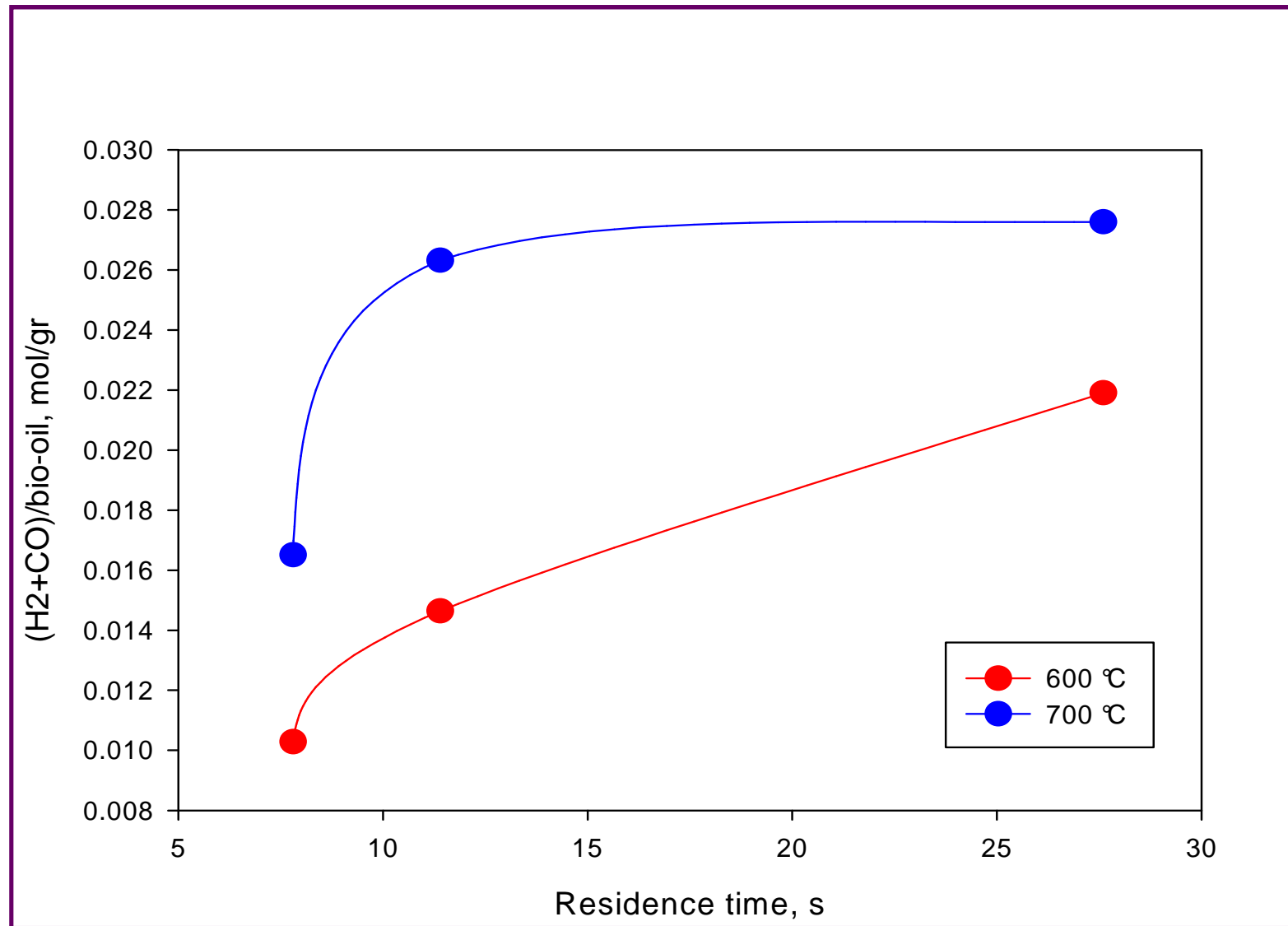


## Experimental conditions

- Atomization and fluidization gas: Nitrogen
- Source of steam: Water in bio-oil
- Temperature: 500 °C - 700 °C
- Pressure: atmospheric
- Two silica sands:  $d_{psm} = 80 \mu\text{m}$  and  $200 \mu\text{m}$
- Mass of bed: 1.5 kg and 3.0 kg
- Residence time varied by changing the reactor volume



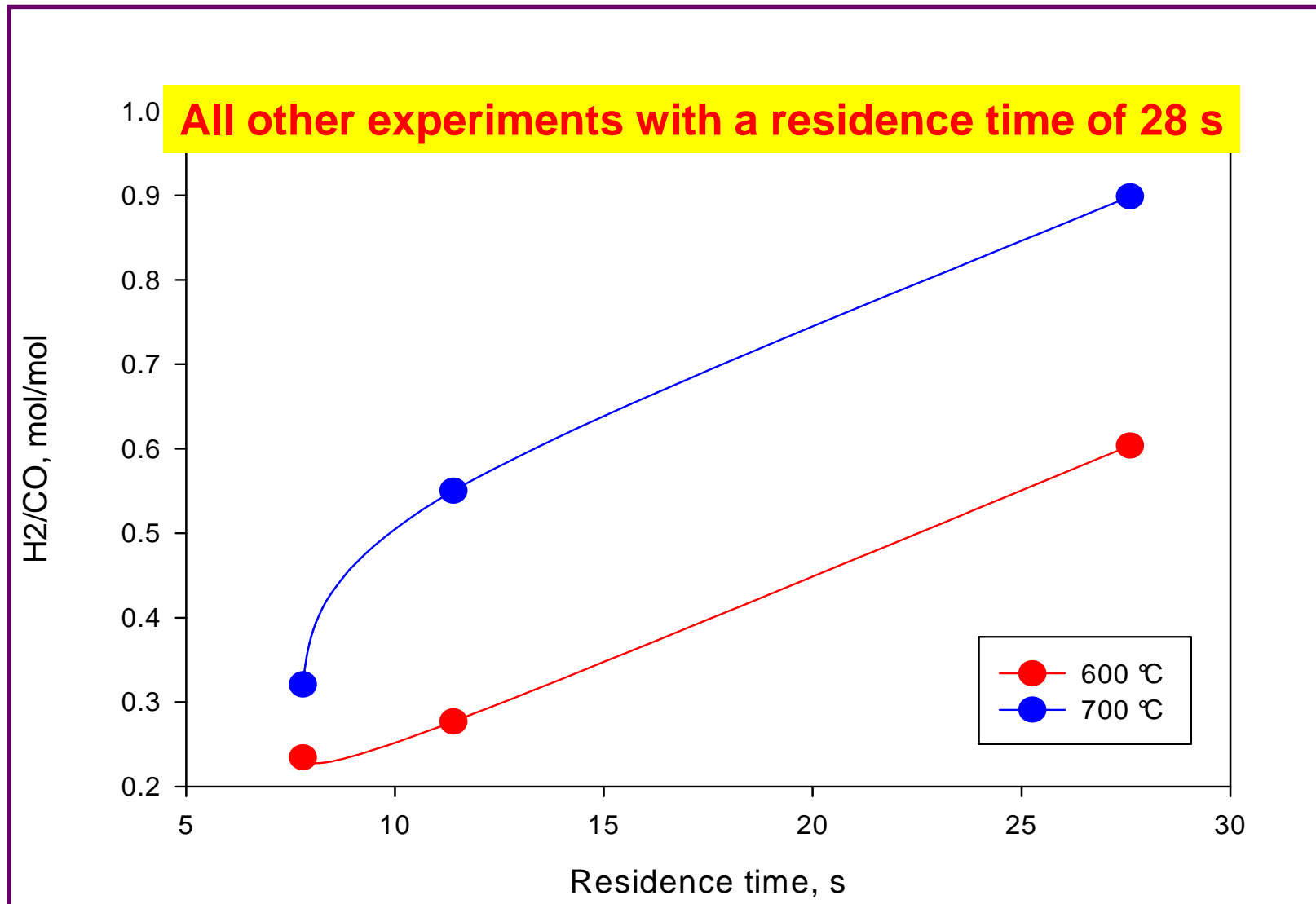
# Experimental results- Effect of Residence Time



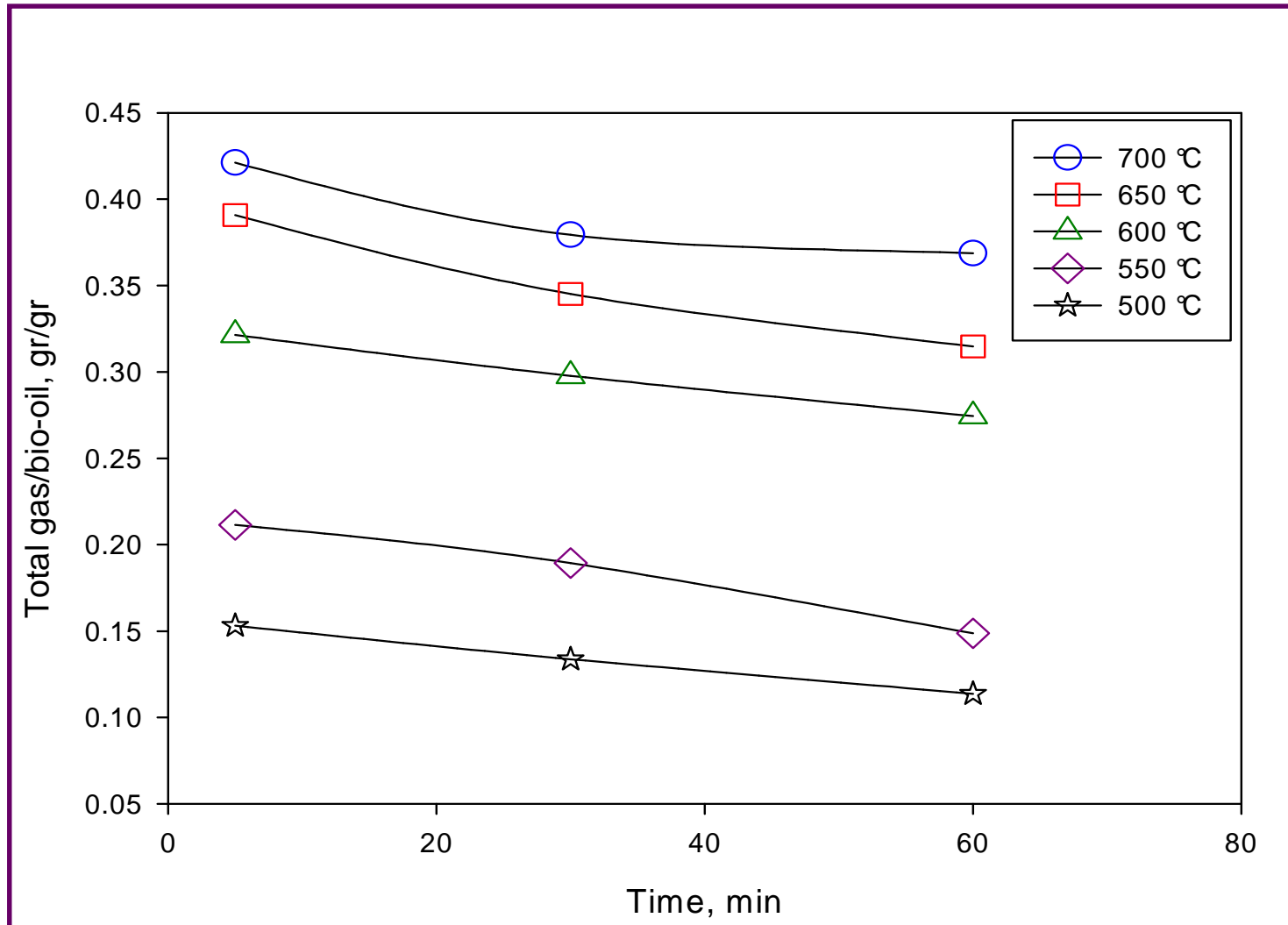
Yield of Syngas ( $\text{H}_2+\text{CO}$ ) for 1.5 kg sand ( $d_{\text{psm}}=200 \mu\text{m}$ )



# Experimental results- Effect of Residence Time

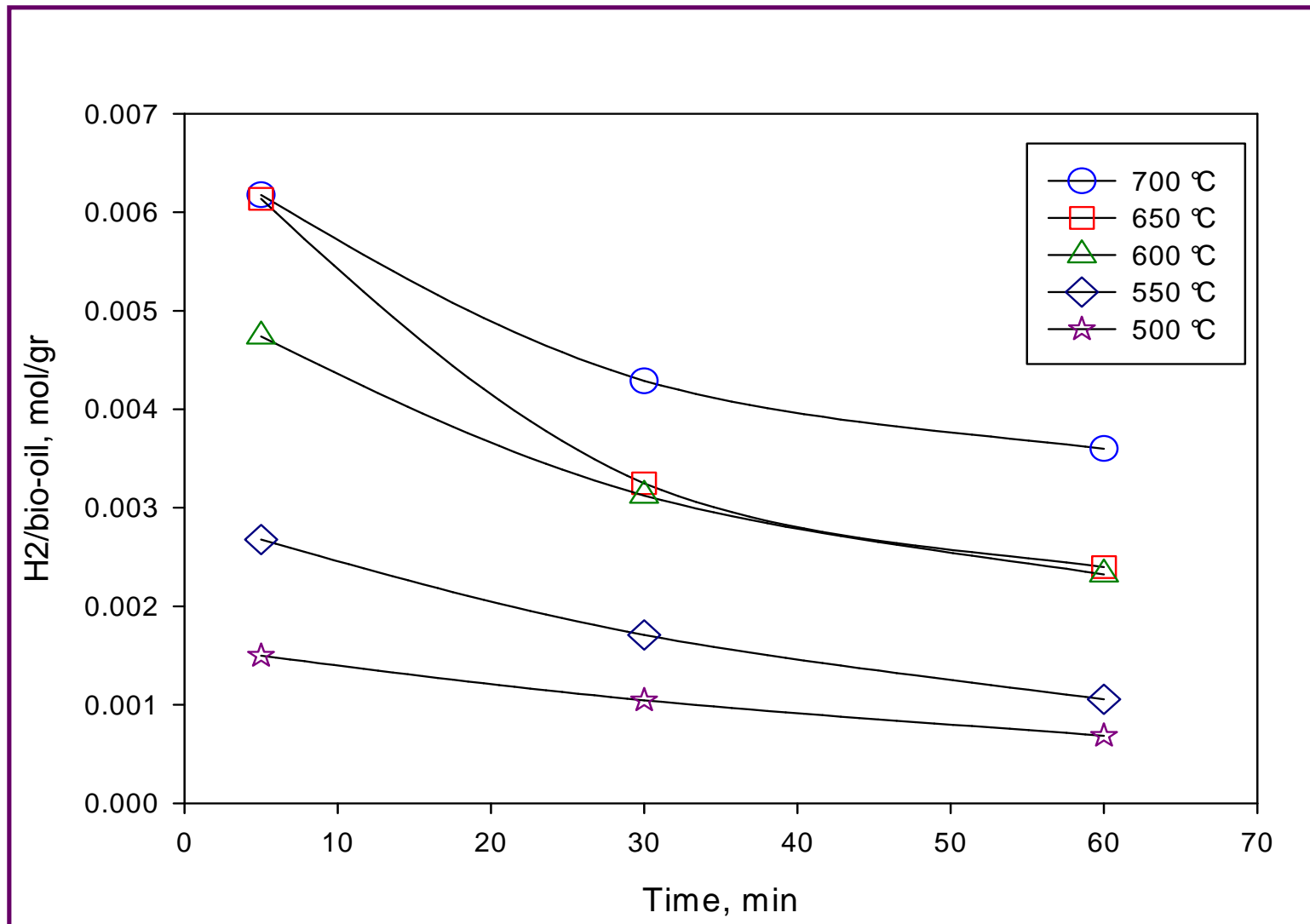


# Experimental results- Effect of Temperature



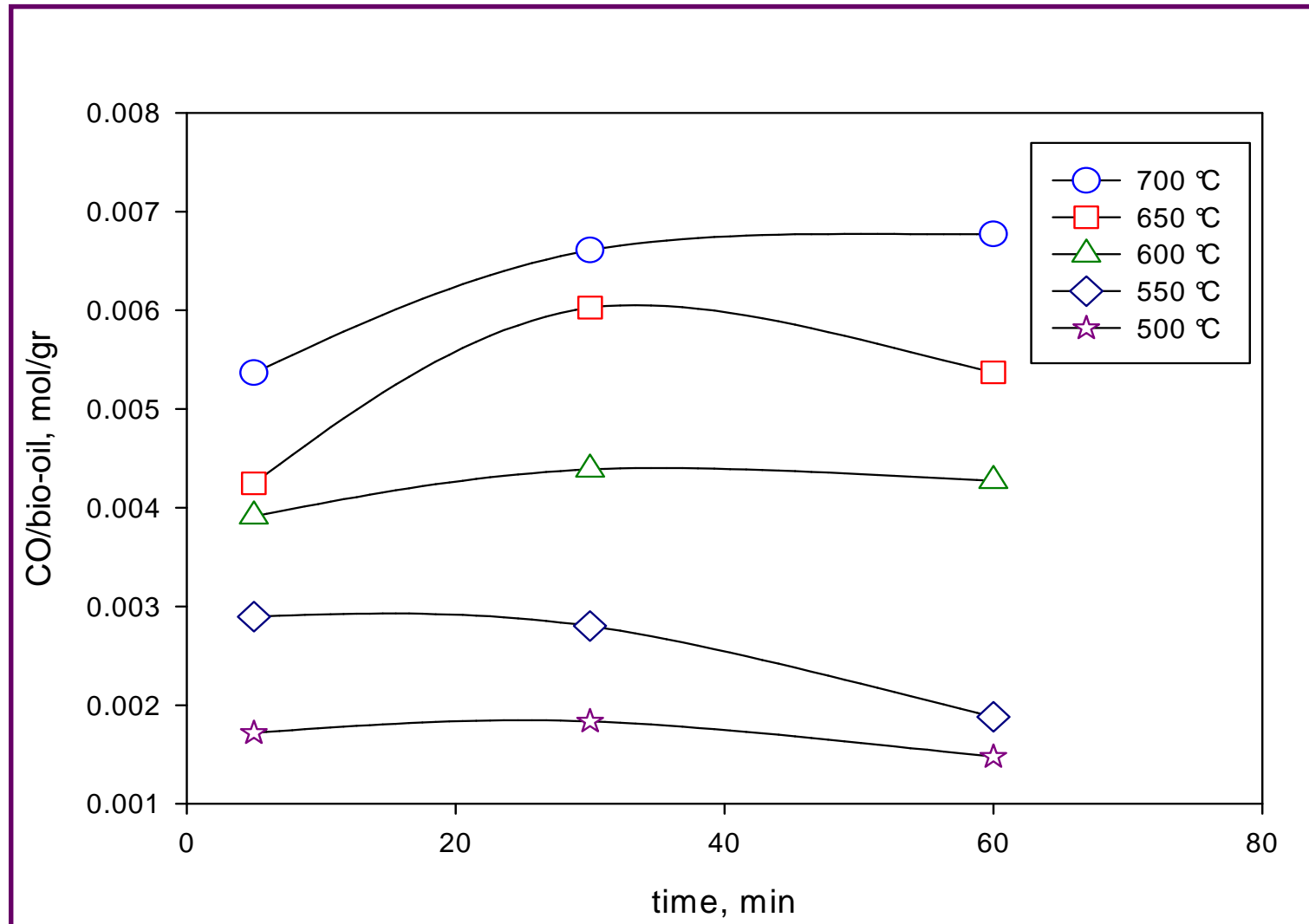
Yield of Total gas (H<sub>2</sub>, CO, CO<sub>2</sub> and CH<sub>4</sub>) for 1.5 kg sand ( $d_{psm} = 200 \mu\text{m}$ )

# Experimental results- Effect of Temperature



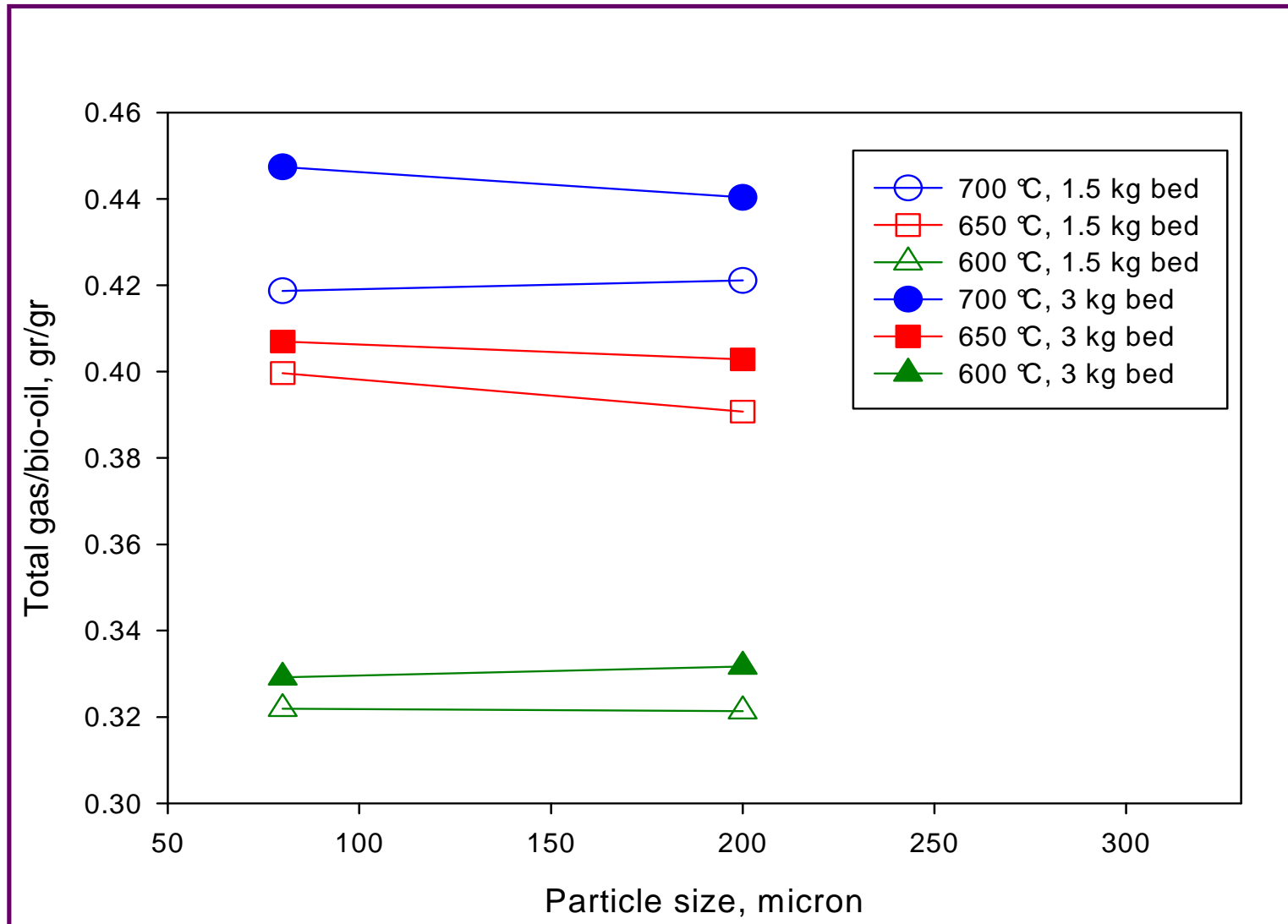
Yield of H<sub>2</sub> for 1.5 kg sand ( $d_{psm} = 200 \mu\text{m}$ )

# Experimental results- Effect of Temperature



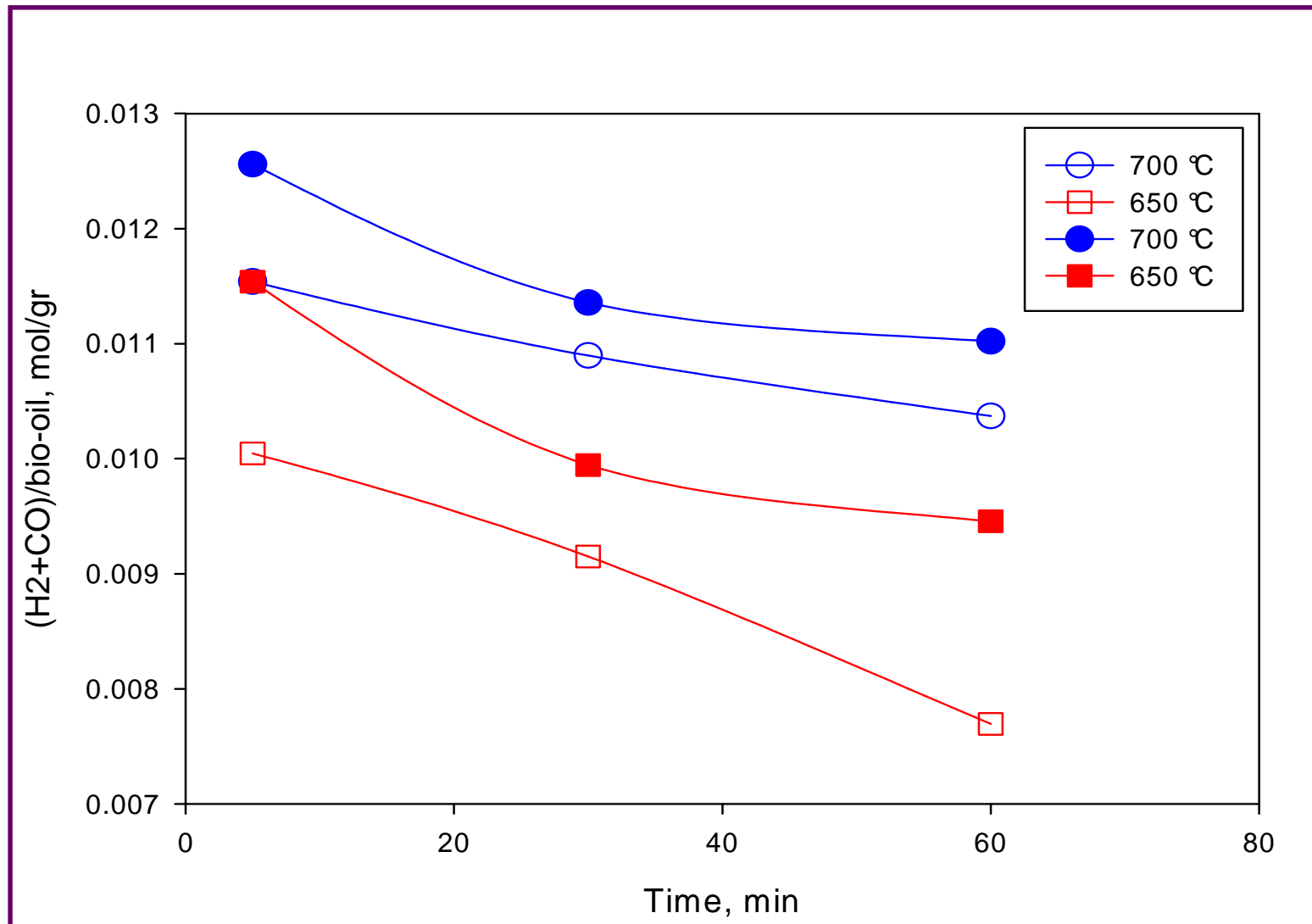
Yield of CO for 1.5 kg sand ( $d_{psm} = 200 \mu\text{m}$ )

# Experimental results- Effect of Particle Size



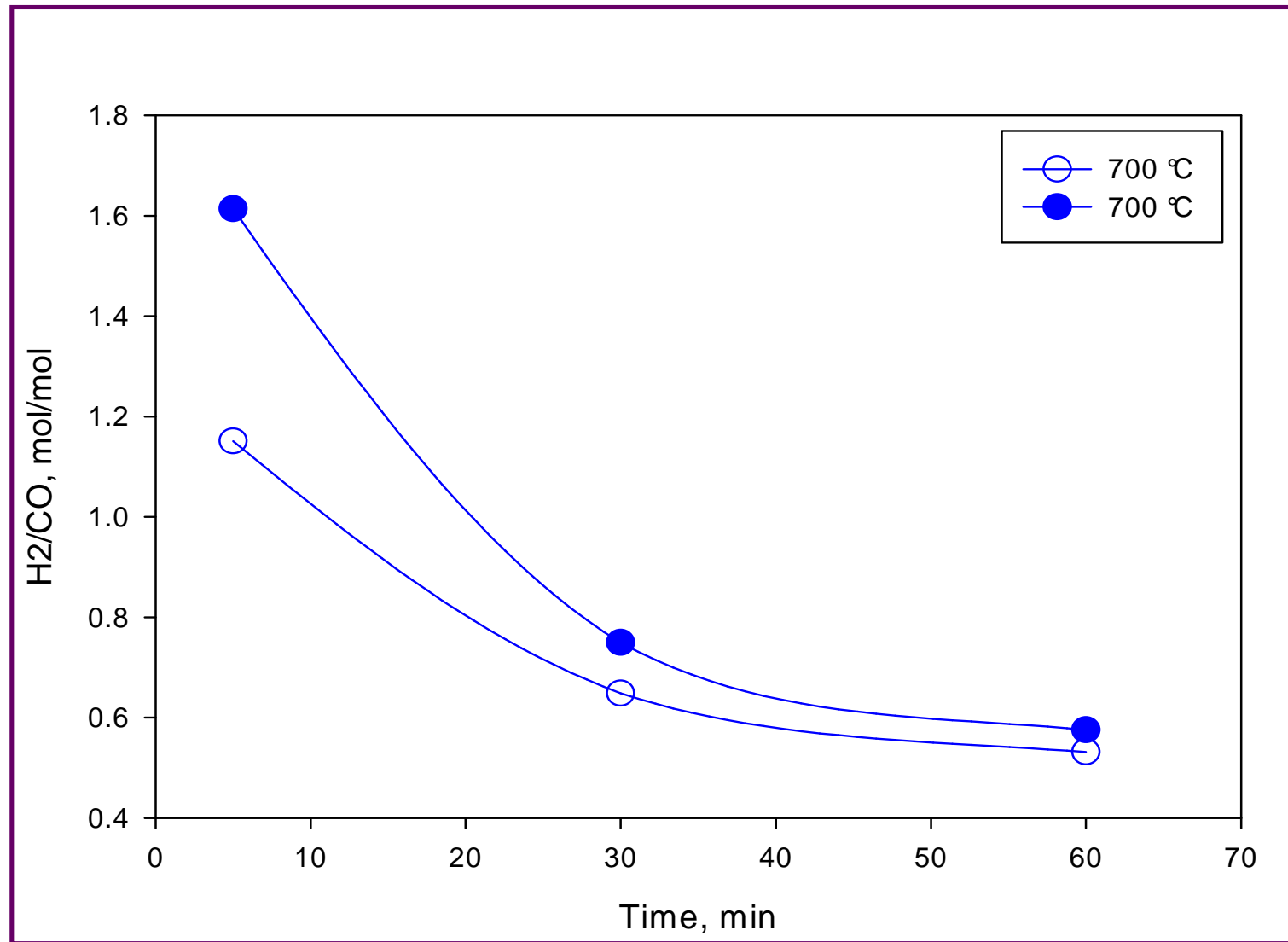
**Yield of Total gas (H<sub>2</sub>, CO, CO<sub>2</sub> and CH<sub>4</sub>)  
for 1.5 kg and 3.0 kg sand beds ( $d_{psm}=80 \mu\text{m}$  and  $200 \mu\text{m}$ )**

# Experimental results - Syngas (H<sub>2</sub>+CO) Production



Yield of syngas for 1.5 kg (open symbols) and 3.0 kg (closed symbols) sand ( $d_{psm} = 200 \mu\text{m}$ )

# Experimental results- H<sub>2</sub>/CO



H<sub>2</sub>/CO molar ratio

**icfar** for 1.5 kg (open symbols) and 3.0 kg (closed) sand ( $d_{psm}=200\mu\text{m}$ )

# Conclusions

- ❑ **Similar results obtained with two particle sizes:**
  - ➔ **sand has no catalytic effect**
  - ➔ **no significant heat or mass transfer limitations**
  
- ❑ **Coke formation:**
  - ➔ **reduction with time of the gasification yield**
  
- ❑ **Longer residence times and higher temperatures**
  - ➔ **better syngas yield and quality**